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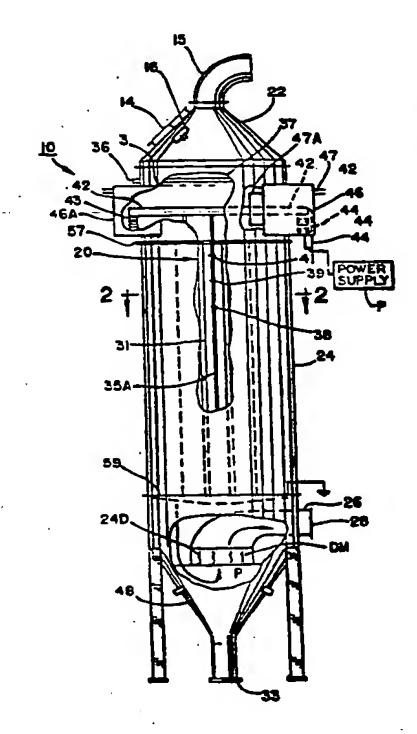
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(54) Title: WET ELECTROSTATIC PRECIPITATOR AND METHOD OF USING SAME

(57) Abstract

A wet electrostatic precipitator (20) having a cylindrical housing (24), an inlet in an upper portion (22), a nozzle (16) for delivering an atomized spray, inner and outer concentric electrodes (35Å, 31) wherein the outer electrode (31) is in the form of a collector tube which is supported by top and bottom plates (57, 59). The inner electrodes (35A) are supported by a bus bar (42) which is connected to a power supply (P). An outlet (28) is connected to the interior of the housing (24).



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Description

WET ELECTROSTATIC PRECIPITATOR
AND METHOD OF USING SAME

Technical Field

The present invention relates generally to an electrostatic apparatus and method for removing particulates from fluid streams. The invention more particularly relates to a new and improved wet electrostatic precipitator, and method of operating same, for more efficient and effective particle removal.

Background Art

Electrostatic precipitators have been employed for removal of particulates in waste fluids. Typically, the precipitators include concentric electrodes in the form of an electrically conductive rod or mast disposed within an electrically conductive collector tube. A high voltage discharge between the electrodes ionizes particles from the waste fluid.

reference may be made to U.S. patents 2,748,888;
4,194,888; 4,389,225; and 4,675,029. While the
precipitators disclosed in the foregoing patents may have
been satisfactory for some applications, they have
suffered from certain drawbacks. In the first place,
conventional electrostatic precipitators require unduly
excessive amounts of electrical energy and are,
therefore, unnecessarily expensive to operate. This is
especially the case when very small particles, in the
submicron range, are to be removed from a waste gas
stream.

In view of the foregoing, it would be highly desirable to have an electrostatic system for removing very small particles from waste gas streams in an efficient manner, without requiring unduly large amounts of power consumption.

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When large volumes of waste gas are being treated, non-uniform and weak electrical fields present an even greater problem. Thus, in large capacity systems for handling large volumes of gas, there is even a greater demand for electrical energy for particle removal purposes. Therefore, it is even more critical to have a highly efficient and effective system.

In general, the conventional electrostatic precipitators described above may be useful with regard to handling large volumes of waste gas. The problem relates to the construction and configuration of the inner electrode. In this regard, the foregoing mentioned prior known electrodes employ various different projections extending along an inner electrode mast, in a spaced apart manner, relative to an outer collection tube. The spacing is critical, and enables the electrostatic discharge to occur between the electrodes. However, the projections, such as helical fins and discs, serve as a hinderance to the free flow of gas through the collection tubes. Additionally, such projections do not provide the highly desirable uniform electrostatic field to increase particle removal from the gas.

In view of the foregoing, it would be highly desirable to have an inner electrode disposed in such a manner relative to the outer electrode to decrease the impedance presented to the flow of gas therethrough, and at the same time provide an extremely uniform high strength electrostatic field.

As a clear example of such a system which fails in both instances, reference may be made to the foregoing U.S. patent 4,675,029, which discloses an electrostatic precipitator having an inner electrode provided with discs having static discharge projections extending radially therefrom. The discs extend radially from the inner mast outwardly toward the inner surface of a

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As a result, the discs present an interference with the free flow of gas through the collection tube, thereby increasing back pressure in an undesirable manner. Even more importantly, the discs are not particularly uniform, and thus an inefficient operation occurs.

Thus, it would be highly desirable to have a new electrode arrangement for an electrostatic precipitator which would increase greatly the efficiency of its operation. In this regard, the inner electrode should not present an undue impedance to the flow of gas through the collection tube, and at the same time, present a highly uniform electrostatic field.

Disclosure of Invention

It is therefore a principal object of the present invention to provide an electrostatic precipitator and method of using it having high intensity ionization electrodes for providing a uniform electrostatic field for more efficient and effective particle removal.

It is a further object of the present invention to provide such an electrostatic precipitator and method for greatly reducing impedance to the flow of fluid to be cleaned through the precipitator.

Briefly, the above and further objects of the present invention are realized by providing a new and improved wet precipitator and method to enable it to be operated more efficiently and effectively.

A wet electrostatic precipitator and method include the use of concentric electrodes, the inner one of which includes a discharge disc extending a short distance therefrom toward the outer electrode to reduce the impedance to waste gas fluid flow. A relatively large number of discharge points on the outer periphery of the disc provides a large number of radially extending discharge paths to the outer electrode, in a very uniform

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manner. In a preferred form, a large number of individual discharge points are utilized to produce a uniform field distribution. The number of discharge points is precisely determined because if the disc were to have too many points, the disc would approach a smooth outer periphery and not be as effective in maintaining a uniform field. Too few points would lead to a condition of fewer individual discharges and less uniformity in the field.

Brief Description of Drawings 10

The above mentioned and other objects and features of this invention and the manner of attaining them will become apparent, and the invention itself will be best understood by reference to the following description of the embodiment of the invention in conjunction with the accompanying drawings, wherein:

FIG. 1 is an elevational, partially cut away diagrammatic view of the electrostatic precipitator of the present invention, the precipitator being illustrated in a waste gas treating system;

FIG. 2 is an enlarged sectional view of the system of FIG. 1, taken substantially on line 2-2 thereof;

FIG. 3 is a greatly enlarged plan view of a discharge disc of the circled portion of the precipitator of FIG. 2:

FIG. 4 is a fragmentary sectional view of another precipitator, which is also constructed according to the invention, and which is shown with only one pair of its concentric electrodes;

FIG. 4A is a fragmentary sectional view of another electrostatic precipitator, which is also constructed 30 according to the present invention, and which is shown with only one pair of its concentric electrodes;

FIG. 5 is a fragmentary sectional view of still another form of a precipitator, which is also constructed 35

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according to the invention and which is shown with only one pair of its concentric electrodes;

FIG. 6 is a fragmentary sectional view of yet still another form of a precipitator, which is also constructed according to the invention and is shown with only one pair of its concentric electrodes; and

FIG. 7 is a greatly enlarged view of the circled portion of the electrode of FIG. 3.

Best Mode for Carrying Out the Invention

Referring now the drawings, and more particularly to FIG. 1 thereof, there is shown a wet scrubbing system 10 having an inlet 11 in an upper portion 22 of a generally cylindrical housing 24 confining a wet electrostatic precipitator 20, which is constructed in accordance with the present invention. Waste gas enters the system 10 at an inlet 11, passes through a cylindrical conduit 13 into the upper portion 22 where the waste gas is saturated with a finely atomized spray of an additive, such as water, delivered by an atomizing nozzle 16 which is held in place by a nozzle plate 14, and which is shown diagrammatically to include a pair of opposed nozzles. The saturated gas then passes into the housing 24.

The electrostatic precipitator 20 produces an electrical field through which the saturated waste gas must pass. During passage, particles in the waste gas become electrically charged. The particles adhere to an oppositely charged electrodes of the precipitator and are thereby removed from the waste gas stream. The waste gas, now cleaned of the particles, passes through a demister DM, having an array of baffles, such as baffle 240, for removing moisture from the treated gas. clean gas generally follows a flowpath P into a cylindrical clean air conduit 26 connecting an outlet 28 to the interior of the housing 24.

During operation, water under pressure is delivered through the atomizing nozzle 16, to saturate the gas. In addition, the water washes particle collecting surfaces, thereby sweeping away particles adhering thereto. The water separated from the gas in the demister DM flows into a funnel shaped portion 48 and, as a sludge containing particles removed from the waste gas stream flows out through a port 33. Water delivery may be continuous or intermittent, depending on particle loading.

Considering now the electrostatic precipitator 20 in 10 greater detail, with reference to FIGS. 1-3, the electrostatic precipitator 20 has a plurality of inner and outer concentric oppositely poled elongated electrodes, such as inner and outer electrodes 35A and 31, respectively, disposed within the interior of the 15 housing 24 and extending in the direction of movement of the sprayed gas flowing therethrough. A power supply P applies a high voltage to the inner electrodes, and the outer electrodes are grounded, to cause a corona discharge to occur between the concentric electrodes. The outer electrodes are all similar to one another, and only the outer electrode 31 will now be described in greater detail. The outer electrode 31 is in the form of an elongated collector tube. The tube 31 is oriented so that the gas flow path through the system 10 is along the 25 longitudinal axis of the electrode. The tube 31 is mechanically and electrically supported between top and bottom plates 57 and 59. The collector tube 31 collects charged particles during system 10 operation. It may have an internal diameter ranging from about 8 inches to 30 about 12 inches. In a preferred system actually constructed, the collector tube 31 has an internal diameter of about 10 inches, and is about ten feet in length. 35

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As best seen in FIG. 1, a bus bar 42 is disposed within the housing 24 and is electrically isolated from connection therewith by insulators, such as the insulator 43. Suspended from the bus bar 42 and electrically connected are the individual like inner electrodes, such as the inner electrode 35A. The inner electrodes are each fixed in concentric alignment with the corresponding collector tubes, and extend from the bus bar 42 terminating at their bottom distal ends (not shown) spaced above the plate 59.

The high voltage power supply P is electrically connected to a power supply input 44 for delivery of negative electrical energy to the bus bar 42 to create an electrostatic field between the inner electrodes and the grounded outer electrode tubes. It has been determined that the system works well with a field strength of about 6KV/cm, for effective particle removal. The ends of the bus bar 42 are positioned within a pair of similar insulator purge boxes 46 and 46A. The insulator box 46 has the power supply input 44, and an inlet 47 through which heated dry air may be delivered into the hollow interior of the box 46 and out its outlet 47A connected in fluid communication with the interior of the housing 24, for purging the box 46 of moisture and for maintaining the bus bar 42 in a substantially dry state. The other box 46A also is purged in a similar manner.

During operation of the system 10, additive introduced through the nozzle 16, flows along the surfaces of the collector tubes, thereby washing away any particles deposited on the surfaces of the electrodes. Thus, in large measure, the system 10 is substantially self cleaning during the particle removal operation. However, the system 10 may be adapted so that the surfaces of the electrodes can be cleaned of particles in an easy and convenient manner, without disassembly of the

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through a plurality of nozzles, such as a nozzle 34. The nozzles, such as the nozzle 34, are connected in fluid communication with a manifold 37 disposed in the upper portion 22 of the housing 24 upstream of the precipitator 20. An external connector 36 is adapted for receiving a water delivery line (not shown) for admitting water or other suitable cleaning liquid under pressure to the manifold 37. The nozzles 34 direct the water, under pressure, downwardly through the interior of the housing 24 for cleaning the system by removing particles from the electrodes.

Considering now the inner electrodes in greater detail, only electrode 35A will now be described since the other inner electrodes are similar to it. As shown in FIGS. 1-3, the electrode 35A is in the form of an electrically conductive elongated rod or discharge mast 32 axially aligned with, and centered disposed within, its collector tube 31. Discharge discs 38, 39 and 41, are mounted on the mast electrode 32, in a spaced apart relationship along the top portion thereof. In the system actually constructed, the discs are spaced at approximately one foot intervals.

The discharge discs 38, 39 and 41 are electrically and mechanically connected to the mast 32 so that the plane of the disc is transverse to the longitudinal axis of the electrode 32. Each discharge disc is thin, and in the constructed system, is approximately 1/8 inch thick. The discs are preferably constructed of noncorrosive electrically conductive material such as stainless steel. It is recognized, of course, that materials such as zirconium and titanium are also suitable.

Considering now the discharge disc 38, for example, in greater detail, with reference to FIG. 3, the disc has a large number of radially extending sharply pointed

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projections or points, such as the points 73 and 77 to enable an individual corona discharge to be established between the radial discharge points and the inner surface of the collector tube. In this manner, a uniformly distributed electrostatic field is established, due to the sharpness of the points and the relatively large number thereof for a given circumference of the disc. Also, the diameter of the disc is only somewhat greater than the diameter of the mast, to provide only a small impedance to the flowing wet gas therepast. Thus, in accordance with the present invention, each discharge disc is able to not only provide a uniformly distributed electrostatic field, but also a low impedance to gas flow. As a result, the precipitator is highly efficient and effective in its particle removing operation

Arcuate shaped interconnecting web portions, such as the portion 75, are concave in shape, and join the discharge points along the peripheral edge of the disc. As shown in FIGS. 3 and 7, each of the points, such as the point 73, has a pair of curved opposite side edges 73A and 73B. As shown in FIG. 7, the side edges 73A and 73B form an included angle T of between 55° and 65°, with a preferred range of 59° to 61° and a most preferred angle of 60°. In the system which was constructed, each of the side edges 73A and 73B has a radius of curvature ranging from about 0.009 inches to about 0.111 inches, with a preferred range of about 0.110 inches.

It has been found that increased system efficiency and economy are achieved when the disc 38 has a large number of points disposed along its periphery. In the constructed system, the disc has 50 points arrayed along the periphery of the disc 38. The corona discharge thus produced is very stable and the electrostatic field is more efficient in particle removal. In addition, field fluctuations are significantly diminished.

The relative dimensions between the discharge disc 38 and the mast electrode 32 are found to be critical. The discharge disc should be sufficiently small to present low impedance to the gas flow around it, yet capable of maintaining a high intensity uniform field. It has been found that in the discharge disc 38, as best seen in FIG. 3, a tip to tip diameter dimension D, is between about 1.575 to about 1.825 times the rod diameter d with a preferred range of about 1.64 to about 1.76, and a most preferred dimension D being about 1.7 times the diameter d. Thus, in the constructed system, the disc 38 has a dimension D of approximately 3.4 inches, while the rod diameter d is approximately 2.0 inches.

It has been found that the 1.7 ratio is critical. If, for example, $\frac{D}{d}$ is too large, the disc presents too 15 high an impedance to gas flow, and thus precipitator efficiency is reduced to an unacceptable level. Also, when the disc diameter is too large for a given diameter mast, sparks (and not the desired corona discharge) are established between the inner and outer electrodes, at too low a voltage. Also, in small diameter masts, 20 relative to the size of the diameter of the disc, unwanted coronal discharges from the mast itself are produced, when, of course, it is desirable that the discharge emanate from the disc electrode. Such discharges or sparks are wasteful of electrical energy 25 and, in addition, lead to an inefficient particle removal operation.

on the other hand, where the disc/mast relationship $\frac{D}{d}$ is too small, inefficient system performance results because the electrostatic field between the disc tip and the tube wall is not readily established and maintained in a desired manner.

Another critical consideration with regard to the precipitator 20 of the present invention is related to the number of discharge disc points 73 per mast circumference inch. It has been found in the constructed system for example, that 50 discharge points per discharge disc are preferred, when D = 3.4 inches and d = 2 inches. In this case, the number n of points per mast circumference inch is about 7.95. While this is a most preferred value for n, it has been found that ranges of 6.2 to 8.8 and 7.6 to 8.4 are also suitable. In the case where system operations may require a mast diameter which is more or less than 2 inches, the desired number n of discharge points per mast circumference inch, can be readily calculated from the formula $n=\frac{50}{\pi d}$ where d is the

15 new mast diameter.

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Considering now the tube electrode 31 in greater detail, with reference to FIGS. 1 and 2, the electrode, in the constructed system, has an inside diameter of ten inches. In this case, a preferable mast diameter is about 2 inches for maintenance of a uniform electrostatic field.

With regard to the radial spacing distance S (FIG. 2) between the collector tube 31 inner wall and the periphery of the discharge disc 38, the formula for a preferred spacing would be:

$$S = D_t - D$$

where S is the distance between a tip of one of the points of the discharge electrode and the inner wall, D_t is the distance between the inner wall and the axis of the mast electrode 32 and D is the maximum point tip to point tip dimension of the discharge disc 38 (FIG. 3). Thus, in the constructed system, the collector tube 31 has an internal diameter of about 10 inches, application

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of the formula reveals that a suitable distance S would be from about 3.0 inches to 3.6 inches with a preferred range being about 3.2 to about 3.4 inches and a most preferred distance about 3.3 inches.

As in the case of the discharge disc 38, the collector tube 31 and the mast 32 are made of suitable corrosion resistant, conductive materials such as stainless steel.

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with reference now to FIG. 4A, there is depicted another precipitator 120, which is also made according to the present invention. The precipitator 120 is generally similar to the precipitator 20, with the exception of the configuration of the collector electrode 131.

In FIG. 4A, there is shown for illustration purposes, only one of a pair of concentric electrodes 135 and 131, respectively. The other like electrode pairs and the other portions of the precipitator 120 are not shown for sake of simplicity.

The inner electrode 135 is similar to the inner electrode 35A of FIG. 1, and includes a mast 132 having spaced apart discharge discs, such as the disc 138, disposed thereon.

The electrode 131 is generally rectangular in cross section throughout its length and is comprised of four walls 141-144. The transverse cross sectional shape is preferably square. While the electrode 131 operates in a generally similar manner to the electrode 31 of FIG. 1, and is generally similar in particle removal function, the configuration of the walls 141-144 render the electrode 131 less expensive to manufacture than the cylindrically shaped electrode 31 of FIG. 1. In this form of the invention, a mast electrode 132 having a discharge electrode 138 mounted thereon is centrally and coaxially positioned within the squared tubular collector electrode 131.

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Referring to FIG. 4, there is shown another electrostatic precipitator 62C which is constructed according to the present invention. The precipitator 62C is generally similar to the precipitator 20 of FIG. 1 in structure and particle removal function, except for the shape of the discharge discs. Thus, only a portion of the disc and the mast are illustrated.

The precipitator 62C includes an inner electrode E having a mast 55C and a discharge disc 38C. A large number of discharge points 81 are arrayed along the peripheral edge of the discharge disc 38C. The discharge points 81 are each defined by a generally curved side edge and a straight side edge to provide an asymmetrical discharge point. For example, a point 82 is defined by a curved side edge 83A and a generally straight side edge 83B.

As previously described with regard to the electrode disc 32 of FIG. 1, it is critical to have a large number of discharge points arrayed around the periphery of the disc. The preferred number of points may be calculated according to the foregoing formula.

Referring to FIG. 5, there is shown yet another electrostatic precipitator 62D which is constructed according to the present invention. The precipitator 62D is generally similar to the precipitator 20 of FIG. 1 in structure and particle removal function, except for the shape of the inner electrode discharge discs.

The precipitator 62D of FIG. 5 includes an inner electrode F having a mast electrode 55D and a discharge disc 38D. The disc 38D includes a plurality of 30 peripherally arrayed, radially extending points 86 disposed on the outer edge of the disc 38D. Each point is defined by a pair of generally straight, unequal length side edges forming a V shaped discharge point. For example, a point 86A includes a side edge 84, which

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is approximately twice the length of its other side edge

In the case of the precipitator 62D and as discussed with regard to the disc electrode 32 of FIG. 1, it is desirable to have a large number of points arrayed around the periphery of the disc 38D. The preferred number of points may be calculated according to the foregoing formula.

As shown in FIG. 6, an electrostatic precipitator 62E is illustrated and is constructed according to the present invention. The precipitator 62E is generally similar to the precipitator 20 of FIG. 1 in structure and particle removal function, except for the shape of the discharge disc.

The precipitator includes an inner electrode I having a mast electrode 55E and a discharge disc 38E. In this form of the invention, the disc 38E includes a plurality of spike shaped discharge points, such as the discharge point 88, extending radially outwardly from the discharge disc 38E in a plane transverse to the axis of the mast electrode 55E. In a preferred embodiment of the precipitator 62E, the length 1 of the spike 86 is approximately equal to the width w of an annular hub H of the disc electrode 38E.

The electrostatic precipitator of the present invention has many significant advantages. In the first place, it produces a high intensity ionizing electrode configuration to concentrate the charging field in the zone between the disc and the collecting tube electrode. Thus, the performance of the system exceeds conventional designs and results in more efficient operation. Further, the disc configuration provides excellent collection of particulate matter over a broad spectrum of sizes.

while particular embodiments of the present invention have been disclosed, it is to be understood that various different modifications are possible and are contemplated within the true spirit and scope of the appended claims. There is no intention, therefore, of limitations to the exact abstract or disclosure herein presented.

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What is claimed is:

An electrostatic precipitator for removing particles from a gas stream comprising:

an inner and an outer electrode;

power supply means for supplying discharge potential between said inner electrode and said outer electrode to cause a corona discharge therebetween;

said inner electrode including an elongated sleeveless one piece unitary mast having a diameter d and a plurality of spaced apart like discharge discs, each of said discs having a number of individual discharge points to provide individual electrostatic discharges between individual points and the outer electrode to form a uniform electrostatic field wherein the number of discharge points per mast circumference inch equals at least substantially $\frac{50}{\pi d}$ where d equals the mast diameter

measured in inches, and wherein a diameter ratio value of $\frac{D}{d}$ is between about 1.6 and about 2.0 where D is the distance measured in inches between diametrically opposed point tips, to provide a thick, sturdy mast for support purposes and to provide a relatively large number of discharge points per mast circumference inch.

- A precipitator of claim 1, wherein $\frac{D}{4}$ is 1.85. 2.
- A precipitator of claim 1, wherein $\frac{D}{A}$ is 1.70. 3.
- A precipitator of claim 1, wherein said outer electrode has an elongated cylindrical configuration and 25 said inner electrode is coaxially and concentrically aligned therewith in a spaced apart relationship therewith.
- A precipitator of claim 1, wherein said outer electrode has an elongated configuration, rectangular in 30 cross section, and said inner electrode is coaxially

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aligned therewith in a spaced apart relationship therewith.

- 6. A precipitator of claim 1, wherein said outer electrode has an elongated configuration, generally square in cross section, and said inner electrode is coaxially aligned therewith in a spaced apart relationship therewith.
- 7. A precipitator of claim 1, wherein said discharge disc has a plane transverse to the axis of said inner electrode.
- 8. An electrostatic precipitator of claim 1, wherein said points are arrayed in a plane transverse to said mast.
- 9. An electrostatic precipitator of claim 4,

 15 wherein said outer electrode has an internal diameter of between 8 and 12 inches.
 - 10. An electrostatic precipitator of claim 4, wherein said outer electrode has an internal diameter of about 10 inches.
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 11. An electrostatic precipitator of claim 1, wherein the distance S between the inner wall of the outer electrode and the tip of a discharge point is calculated from the formula S = D, D where D, is the distance between said inner wall and the axis of the mast.
 - 12. An electrostatic precipitator of claim 1, wherein said outer electrode is generally rectangular in cross section.
- 13. (Amended) A method of precipitating particles
 30 from a gas stream comprising:

using an electrostatic precipitator having inner and outer electrodes, the inner electrode including a mast having a diameter d, and a plurality of like discharge discs, each of said discs having a number of individual discharge points wherein the number of

discharge points per mast circumference inch equals at least substantially $\frac{50}{\pi d}$ where d equals the mast diameter

measured in inches, and wherein a diameter ratio value of $\frac{D}{d}$

is between about 1.6 and about 2.0 where D is the distance measured in inches between diametrically opposed point tips;

establishing an electric discharge potential between the inner and outer electrodes;

flowing the gas stream under pressure through
the electrostatic discharges to cause unwanted particles
to become electrically charged; and

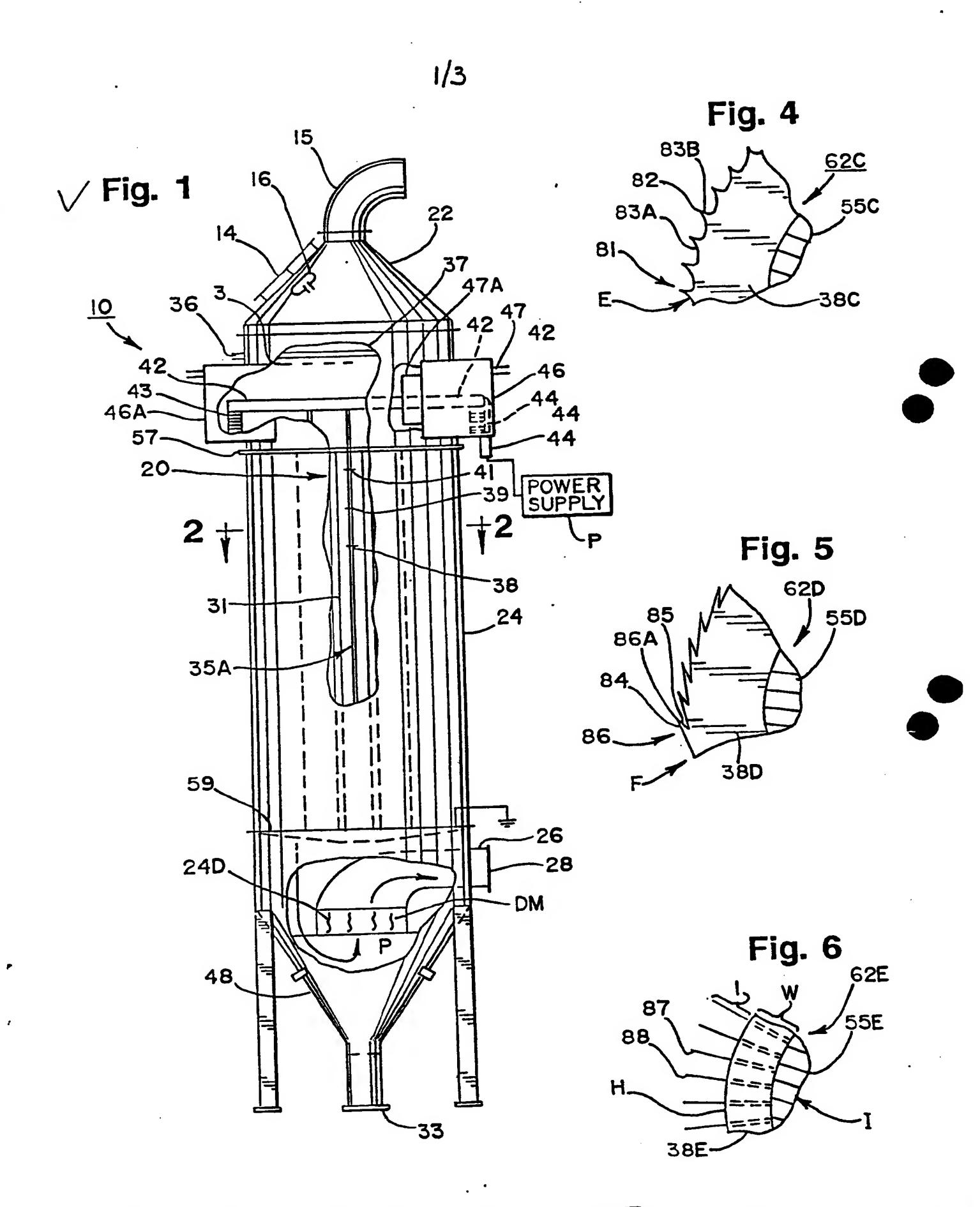
removing the charged particles from the gas stream.

- 14. A method according to claim 13, further including forming a particle containing sludge and removing the sludge from the precipitator.
 - 15. A method according to claim 13, including providing an electrical field strength of about 6KV/cm between the inner electrode and the outer electrode.
- 16. A method according to claim 13, including saturating the gas stream with moisture.
 - 17. A precipitator according to claim 1, including means for saturating the gas stream.
- 18. A precipitator according to claim 1, including means for providing electrical energy to said inner electrode to cause a coronal discharge between the inner electrode and the outer electrode.
 - 19. A precipitator according to claim 1, including a housing, a bus bar disposed within said housing and means for electrically isolating the bus bar from the housing wherein the bus bar is electrically connected to said inner electrode.

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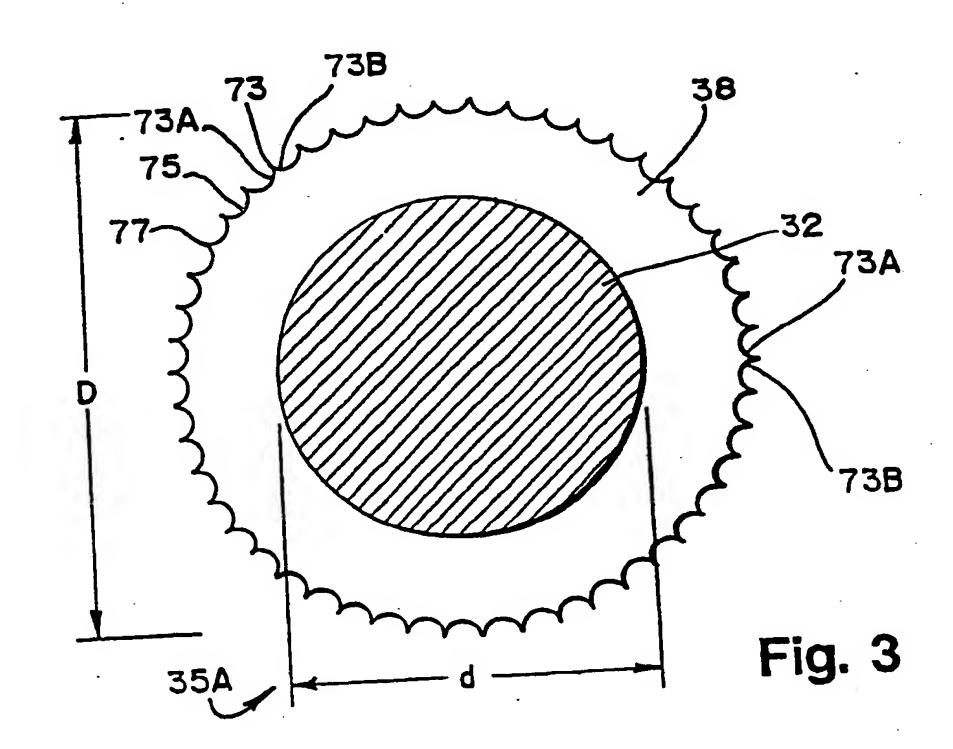
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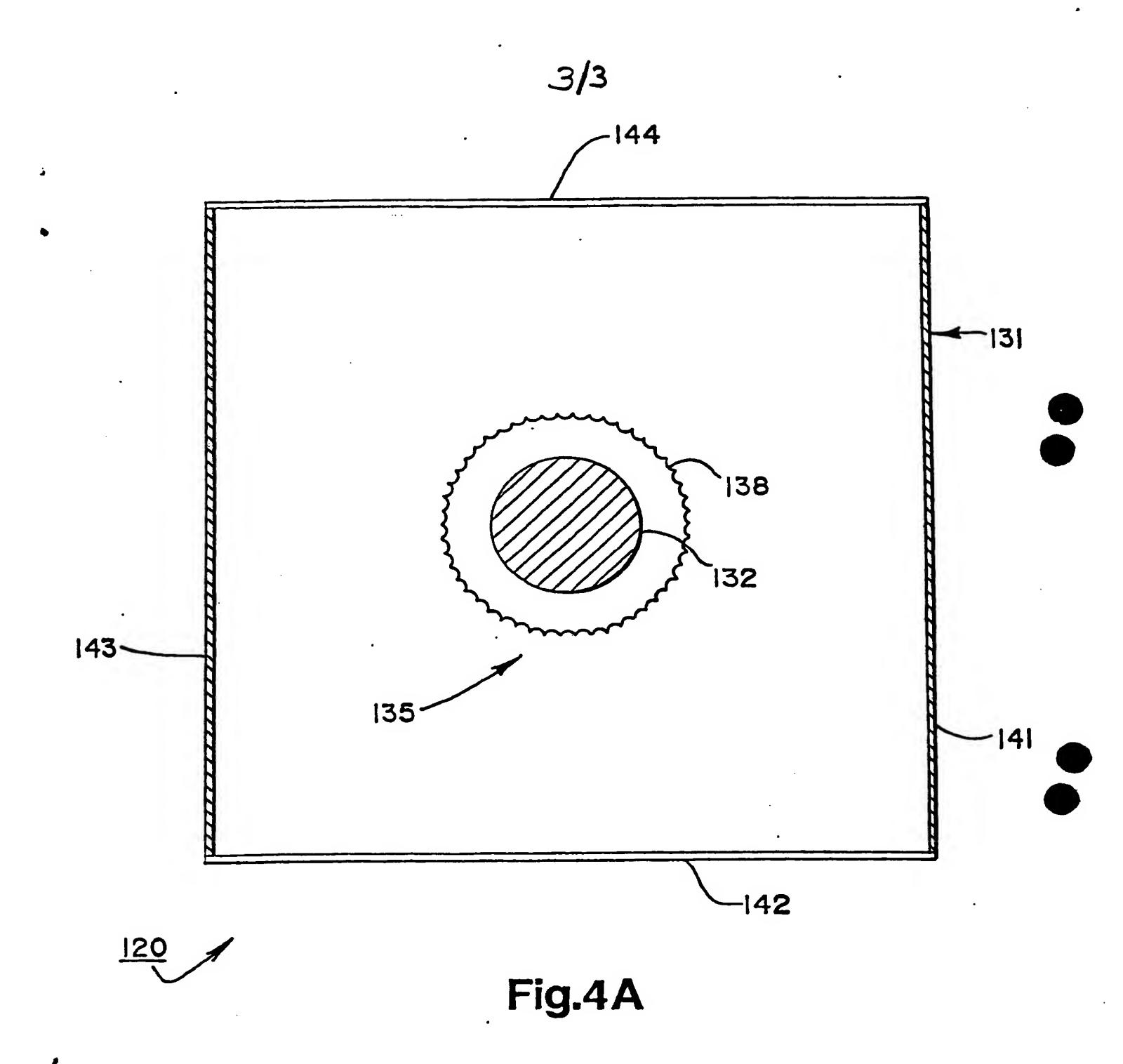
- 20. A precipitator according to claim 19, including means for maintaining the bus bar in a substantially dry state.
- 21. A precipitator according to claim 20, including means for flowing heated dry air under pressure over the bus bar for maintaining it in a substantially dry state.
 - 22. A precipitator according to claim 1, wherein each of said discharge points has a pair of curved opposite side edges, said edges forming an inclined angle of between 55° and 65°.



SUBSTITUTE SHEET

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INTERNATIONAL SEARCH REPORT

International application No. PCT/US92/02999

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| Category* | Citation of document, with indication, where appropriate, of the relevant passages | Relevant to claim No. |
| X | US, A, 4,247,307 (CHANG) 27 January 1981, See figures 2 and 6a. | 1-22 |
| Y. | US, A, 4,194,888 (SCHWAB ET AL) 25 March 1980, See column 4, lines 17-23. | 1-22 |
| Y | US, A, 4,389,225 (WILLETT ET AL) 21 June 1983, See column 2, lines 26-49. | |
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| | ther documents are listed in the continuation of Box C. See patent family annual documents are listed in the continuation of Box C. | |
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